



# OCTAVIUS

OPTIMISATION OF CO<sub>2</sub> CAPTURE  
TECHNOLOGY ALLOWING VERIFICATION  
AND IMPLEMENTATION AT UTILITY SCALE

## Methodology for benchmarking in the OCTAVIUS project

(Sören Ehlers, TUHH)

# Project Background

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- **Different processes have been evaluated during OCTAVIUS with both different solvents and process configurations by various partners**
- **Benchmarking cases are used as a common reference to be able to compare them to each other**
- **In Task 13.1 a framework for these benchmarking cases has been established**

# Project linkages

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- **Task 13.4: Benchmarking**
- **Task 13.2: Optimisation studies (optimised cases with MEA and AMP+PZ as solvents)**
- **Task 25.3: Alternative flowsheets (various flowsheet modifications from literature)**
- **Task 34.4: DMX-1<sup>TM</sup> evaluation study for bituminous coal case (solvent which demixes into two phases)**

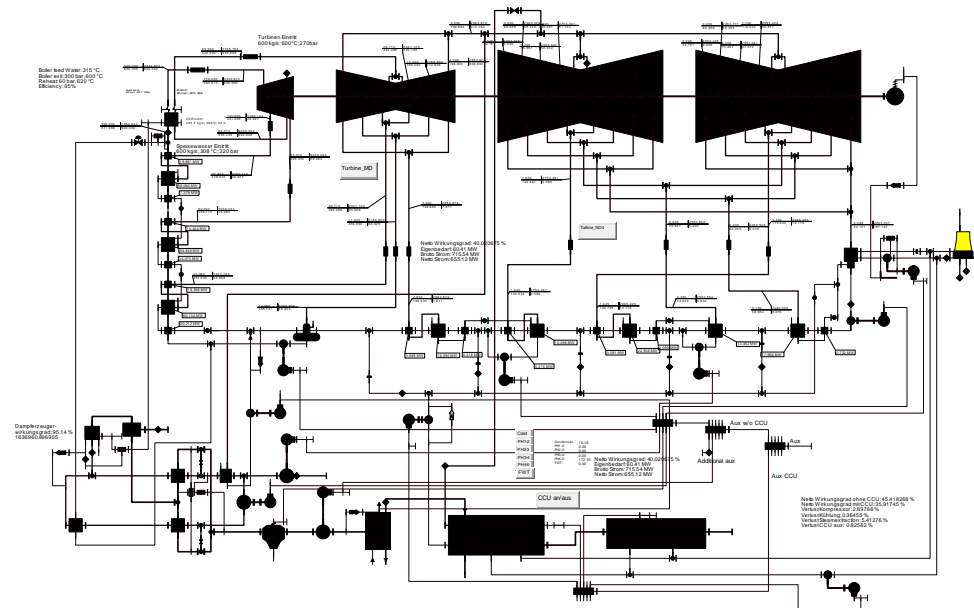
# Reference cases

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- **Reference cases were established using many assumptions from EBTF guidelines**
- **EBTF: European Benchmarking Task Force - Partners from CAESAR, CESAR and DECARBit**
- **Power plant simulation with Epsilon Professional at TUHH**
- **Capture plant simulation with CO2SIM by Sintef**
- **Cost estimation by TNO**

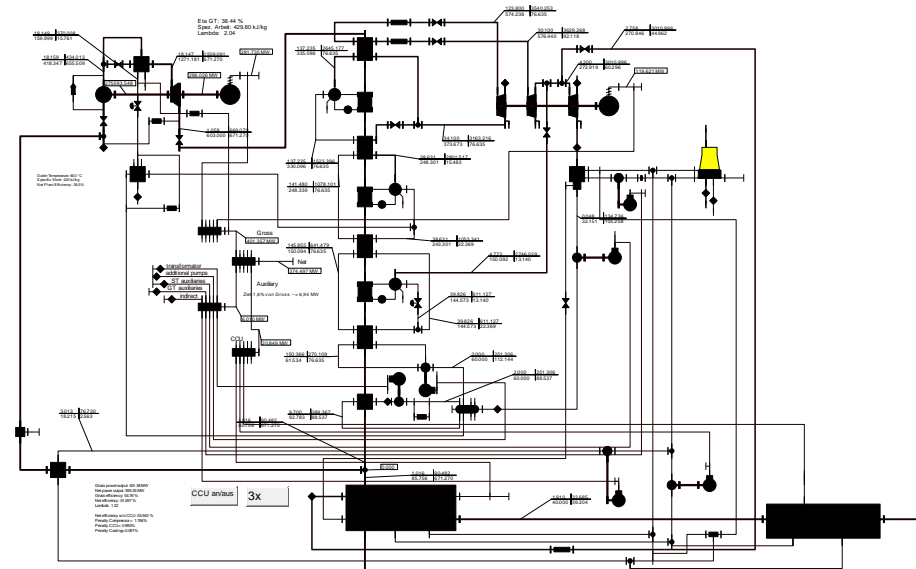
# Bituminous coal reference power plant

- 800 MW<sub>e</sub> bituminous coal case with advanced super critical boiler (ASC)
- 45.4% net efficiency
- 300 bar, 600°C live steam
- 60 bar, 620°C RH steam



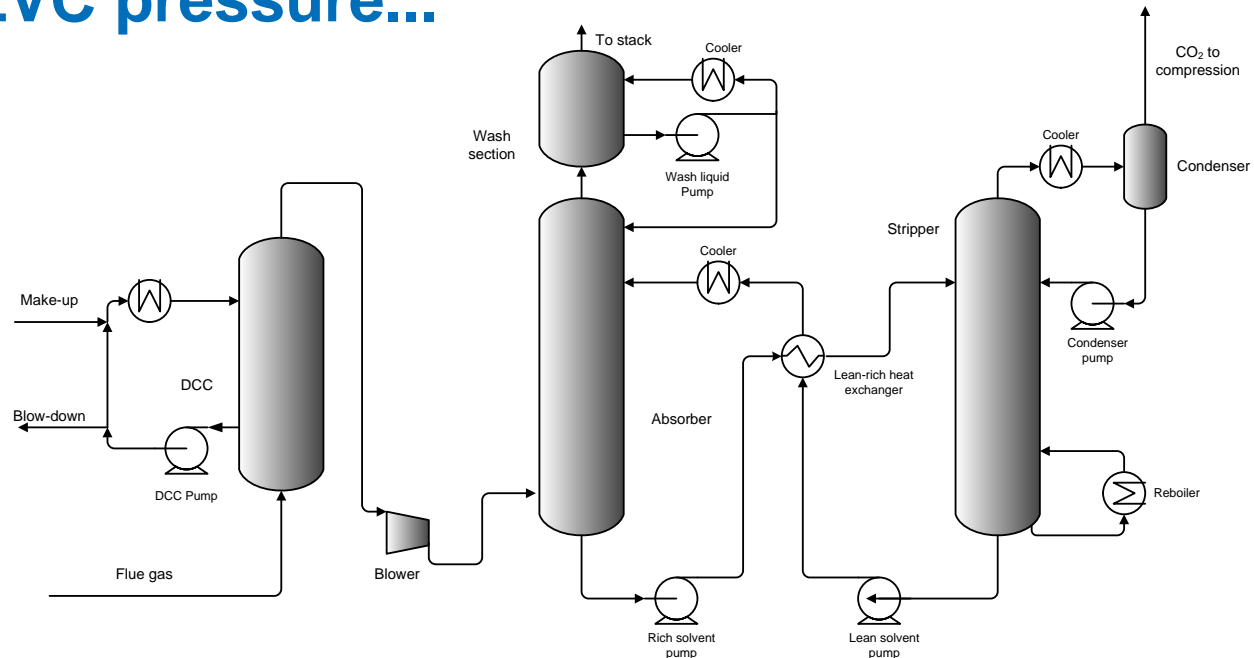
# Natural gas reference power plant

- 430 MW<sub>e</sub> natural gas combined cycle plant
- 57.8% net efficiency
- One gas turbine with one heat recovery steam generator (HRSG)
- Three pressure level HRSG



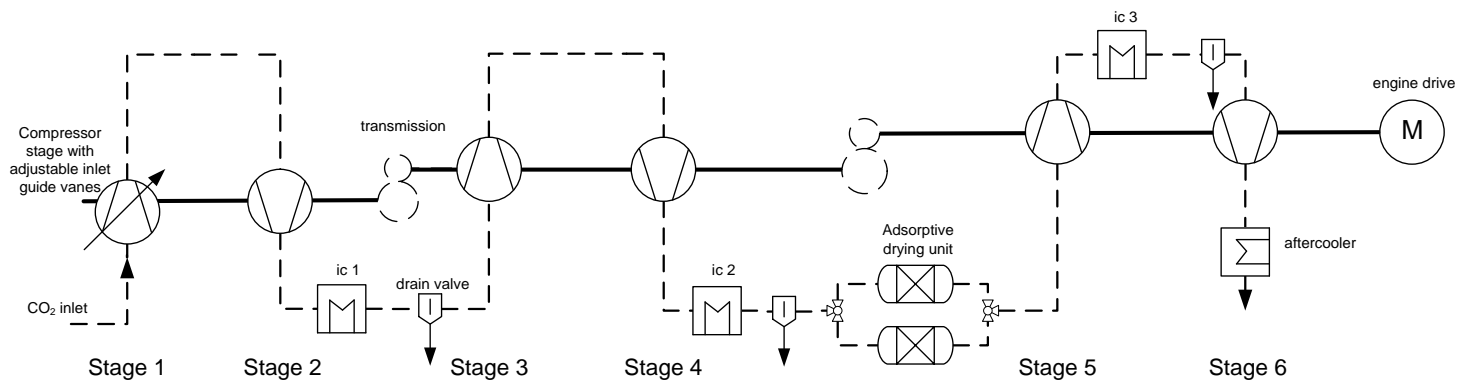
# Reference case - Capture plant

- Modelled by SINTEF
- Optimised during Task 13.2
- Varied parameters: Solution flowrate, absorber height, LVC pressure...



# Reference case - Compressor

- Modelled by TUHH
- Number of stages depends on CO<sub>2</sub> inlet pressure
- Different configurations with intercoolers were evaluated for heat integration potential





# Reference case - Overview

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- **Four reference cases were established**
  - **Coal power plant with 30wt% MEA**
  - **Coal power plant with CESAR I (AMP+PZ)**
  - **Natural gas combined cycle plant with 30wt% MEA**
  - **Natural gas combined cycle plant with CESAR I**

# Benchmarking criteria

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- **Quantitative criteria**
  - **Overall net efficiency penalty**
    - **Specific heat duty**
    - **Specific auxiliary duty**
    - **Specific cooling duty**
    - **Stripper pressure**
    - **Available waste heat sources**
  - **Costing**
    - **Cost of electricity**
    - **Cost of CO<sub>2</sub> avoided**

# Benchmarking criteria - Quantitative

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## ■ Quantitative criteria

### ■ Specific heat duty

- Reboiler heat duty provided by steam from IP/LP crossover
- Electric gross output of power plant is reduced

→ Overall net efficiency is reduced

# Benchmarking criteria - Quantitative

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- **Quantitative criteria**
  - **Specific auxiliary duty**
    - **Flue gas blower and pumps in the capture plant need electricity**
    - **Electric net output of power plant is reduced**
  - **Overall net efficiency is reduced**

# Benchmarking criteria - Quantitative

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## ■ Quantitative criteria

### ■ Specific cooling duty

- Several heat exchangers in the capture plant have to be cooled with cooling water
- Additional cooling water pumps need electricity
- Electric net output of power plant is reduced

→ Overall net efficiency is reduced

# Benchmarking criteria - Quantitative

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## ■ Quantitative criteria

### ■ Stripper pressure

- Stripper pressure determines the pressure ratio for CO<sub>2</sub> compressor and thus electricity consumption
- Electric net output of power plant is reduced
- Stripper pressure determines the evaporation temperature in the stripper and thus required temperature for steam

→ Overall net efficiency is reduced

# Benchmarking criteria - Quantitative

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## ■ Quantitative criteria

### ■ Available waste heat sources

- Certain waste heat sources can be used to heat up feed water
- Less steam has to be extracted from turbine for feed water preheating
- Electric gross output of power plant is increased

→ Overall net efficiency is increased

# Benchmarking criteria - Quantitative

- **Quantitative criteria**
  - **Overall net efficiency penalty**
    - **Total loss in efficiency due to the different mechanisms**
    - **List of mechanisms for MEA base case with LVC**

Mechanism	Efficiency penalty
Steam extraction	5.60 %-points
Compressor duty	3.29 %-points
Cooling water duty	0.29 %-points
Auxiliary power duty	2.04 %-points
Heat integration	-0.76 %-points
<b>Overall efficiency penalty</b>	<b>10.46 %-points</b>



# Benchmarking criteria - Quantitative

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## ■ Quantitative criteria

### ■ Costing

- Cost of electricity calculated for reference power plant
- Detailed calculation of capture plant cost, both CAPEX and OPEX, based on capture plant modeling
- Cost of electricity for overall process (power plant + capture plant + CO<sub>2</sub> compressor)
- Cost of CO<sub>2</sub> avoided:

$$\frac{COE_{capture} - COE_{reference}}{CO_2 Emission_{reference} - CO_2 Emission_{capture}}$$

# Benchmarking criteria - Qualitative

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- **Qualitative Criteria**
  - **Emissions to air and water**
  - **Flexibility**
  - **Dynamics and control**

# Benchmarking criteria - Qualitative

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## ■ Qualitative Criteria

### ■ Emissions to air and water

- Vapour and aerosol emission
- Possible pollutants are among others:
  - Amines
  - Ammonia
  - Nitrosamines
- One of the main topics in OCTAVIUS (WP 1.2: Basic emission control studies)
- Degradation products are contained in waste water as well

→ For benchmarking the different solvents are ranked based on results from other tasks; required counter-measures are included into cost calculation

# Benchmarking criteria - Qualitative

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## ■ Qualitative Criteria

### ■ Flexibility

- In OCTAVIUS Task 24.2 four different operation concepts were evaluated (e.g. exhaust gas bypass and solvent storage)
- Simulations for MEA only
- Results shall be transferred in a qualitative manner to different solvents and process configurations

# Benchmarking criteria

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## ■ Qualitative Criteria

### ■ Dynamics and Control

- **Controllability is affected by complexity of capture plant**
- **Complexity increases costs and reduces availability**
- **Complexity is rated based on**
  - number of incidences of heat- and process integration with power plant
  - number of recycle loops

# Summary

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- **Benchmarking one of the final Tasks in OCTAVIUS**
- **Four reference cases were defined**
- **Different process configurations and solvents are compared**
- **A number of benchmarking criteria are used, both quantitative and qualitative type**

# Reference power plants

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**Thank you for your attention!**